



Radiation Effects in a Semitransparent Gray Coating Heated by Convection and Cooled by Radiation

Charles M. Spuckler
Glenn Research Center, Cleveland, Ohio

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RADIATION EFFECTS IN A SEMITRANSSPARENT GRAY COATING HEATED BY CONVECTION AND COOLED BY RADIATION

Charles M. Spuckler
National Aeronautics and Space Administration
Glenn Research Center
Cleveland, Ohio 44135

ABSTRACT

A parametric study using a one dimensional model of a semitransparent gray thermal barrier coating was performed to gain an understanding of the role thermal radiation can play in the heat transferred. Some ceramic materials are semitransparent in the wavelength ranges where thermal radiation is important. Therefore, absorption, emission, and scattering of thermal radiation can affect the heat transfer through the coating. In this paper a one dimensional layer was used to model the heat transfer process occurring in a burner test rig. The semitransparent layer is heated by a hot gas flowing over its surface. The layer and substrate are cooled by radiation to the surroundings. The back side of the substrate is insulated. The coating is assumed to be gray (absorption and scattering coefficients are not function of wavelength). An absorption coefficient of 0.3 cm^{-1} and scattering coefficients of 0 (no scattering) and 100 cm^{-1} (isotropic scattering) were used. The thickness and thermal conductivity of the layer are varied. The results show that the temperatures are affected by the properties of the semitransparent layer and the emissivity of the substrate. The substrate and surface temperatures are presented. The apparent temperature an optical pyrometer would read for the emitted energy is also given. An apparent thermal conductivity was calculated for the layer.

INTRODUCTION

Some thermal barrier coatings (TBCs), such as zirconia are partially transparent to thermal radiation refs. 1 and 2. In semitransparent materials, both thermal radiation and heat conduction determine the temperature and energy transferred. The radiation heat transfer depends on the absorption and scattering coefficients, and the refractive index of the material. The emission inside the material depends on the refractive index squared. Since the energy that passes through an interface cannot exceed that of a black body some of the energy inside the material is totally reflected back into the layer. This can have a significant effect on the temperatures in the material. An effective thermal conductivity, which includes both conduction and radiation, depends on a number of factors, such as substrate emissivity, the absorption and scattering properties, temperature level and gradient, and the temperature of the surroundings. Determining a single value for the effective thermal conductivity, that can be used for all conditions may not be possible. To determine the heat transferred through a semi-transparent TBC, the conduction equation using the intrinsic thermal conductivity along with the radiative transfer equation or an approximate form of the radiative transfer equation should be used. The work on heat transfer in semitransparent materials with index of refraction greater than one has been reviewed partially in refs. 3 and 4. In these papers the thermal behavior of absorbing, emitting and scattering materials with refractive indices greater than one are predicted. In refs. 5 and 6 approximate solutions were developed.

To design more effective TBCs the roles surface reflections, absorption, emission, and scattering along with heat conduction play in heat transfer must be understood. To determine these effects, the absorption and scattering coefficients, and refractive index of the material as a function of wavelength and temperature must be known. The scattering characteristics of the TBC will depend on the structure of the material. The intrinsic thermal conductivity also has to be determined.

A burner test rig is often used to evaluate TBCs. To obtain an understanding of how radiation affects a TBC in a burner rig test, a semitransparent material with absorption coefficient, $a = 0.3 \text{ cm}^{-1}$, scattering coefficients, $\sigma_s = 0$ (non-scattering idealized structure) and $\sigma_s = 100 \text{ cm}^{-1}$ (scattering splat structure) and a refractive index, $n = 2.1$, is considered. These values are in the range of those for zirconia in the wavelengths where it is semitransparent, refs. 1 and 2. The absorption and scattering coefficients, refs. 1 and 2, were determined from experimental data and are a function of wavelength. In ref. 2, data were obtained at temperatures up to 699 K. The scattering coefficient does vary significantly with wavelength. The scattering coefficient, ref. 2, was highest over 300 cm^{-1} near $0.7 \text{ }\mu\text{m}$ and decreased to about 18 cm^{-1} at $5 \text{ }\mu\text{m}$. For this analysis, the TBC is assumed to be gray, the absorption and scattering coefficients and refractive index are not functions of wavelength. The intrinsic thermal conductivity and the thickness of the layer are varied. The substrate and TBC surface temperatures are presented. The apparent temperature an optical pyrometer would measure from the emitted energy is also given for a gray layer. An effective thermal conductivity is calculated using the TBC surface and substrate temperatures. The effective thermal conductivity is compared to the intrinsic thermal conductivity used in the calculations.

MODEL

The model used, fig. 1, is a semi-infinite insulated flat surface coated with a semitransparent

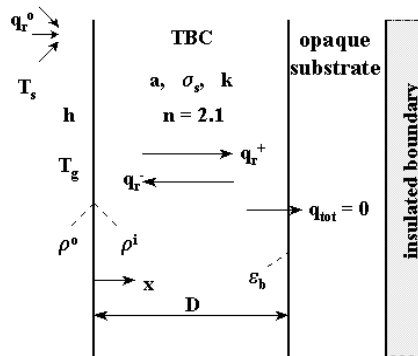


Fig. 1 Heat transfer model

material. A two flux method to examine the effect of various parameters on the thermal behavior of a semitransparent coating on a opaque substrate insulated on its back side was derived in ref. 7. The coating is heated by convection and cooled by radiation. The interface reflections are diffuse. A non-dimensional parametric study was performed in ref. 7 to determine the effects of various parameters on the heat transfer characteristics of the coating. That parametric study is extended to a burner rig test. The equations used from ref. 7 are in appendix A. The prediction of the thermal behavior of a TBC depends on how accurate the thermal and radiative properties are known.

The coating is heated by a gas, $T_{\text{gas}} = 1600 \text{ K}$, flowing over its surface. The convective heat transfer coefficient, h , is $100 \text{ W/(m}^2\text{K)}$. This heat is conducted through the coating to the substrate. The heated coating radiates to itself, the surroundings, and the substrate. There is no heat transfer

through the insulated substrate. Heat is removed by radiation from the layer and substrate to the surroundings $T_s = 295$ K. If the optical thickness, $\kappa_D = (\sigma_s + a)D$, of the layer is small, the layer and substrate will radiate energy to the surroundings. If the layer is optically thick, only volumes near the gas-TBC interface will radiate to the surroundings.

EFFECT OF LAYER THICKNESS AND THERMAL CONDUCTIVITY

The effects of coating thermal conductivity and layer thickness are shown in figures 2 and 3. The

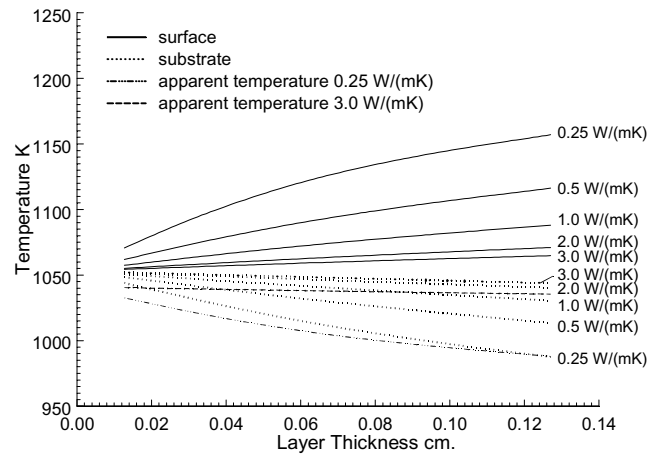


Fig. 2 Surface and substrate temperatures as a function of layer thickness $a = 0.3\text{cm}^{-1}$, $\sigma_s = 0$, $\epsilon_b = 0.8$, and $n = 2.1$

emissivity of the substrate, ϵ_b is 0.8. Figure 2 is for no scattering. The surface temperature (solid lines) increases and the substrate temperature (dotted lines) decreases with thickness. For a given thickness, the surface temperature decreases and the substrate temperature increases as the thermal conductivity increases. For a 0.0127 cm (0.005 in.) thick layer the temperature drop through the layer is 2.3 K for $k = 3.0$ W/(mK) and 26.7 K for $k = 0.25$ W/(mK). For a 0.127 cm (0.05 in.) thick layer the temperature drop through the layer increases to 21.0 K for $k = 3.0$ W/(mK) and 169.5 K for $k =$

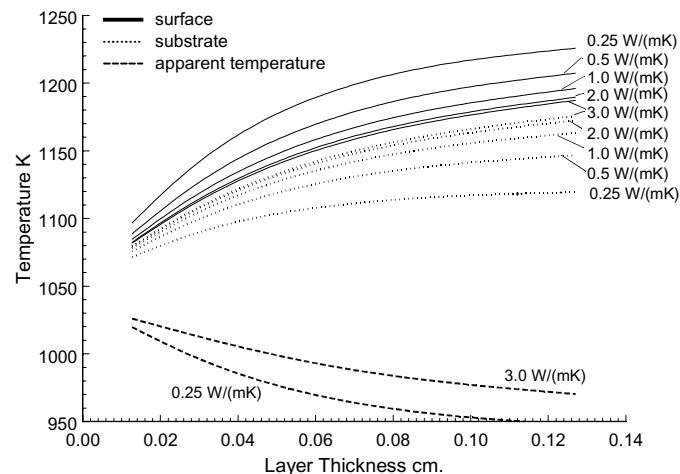


Fig. 3 Surface and substrate temperature as a function of layer thickness $a = 0.3\text{ cm}^{-1}$, $\sigma_s = 100\text{ cm}^{-1}$, $\epsilon_b = 0.8$ and $n = 2.1$

0.25 W/(mK). The temperature profiles in figure 2 are nearly linear for high thermal conductivities indicating conduction may be the dominate mode of heat transfer in the semi-transparent layer. For low thermal conductivities, the temperature curves become non-linear indicating radiation is playing a role in the heat transfer inside the TBC.

Isotropic scattering, $\sigma_s = 100 \text{ cm}^{-1}$ is added in figure 3. Scattering increased the temperature in the layer. Radiant energy emitted by the substrate and the layer is scattered in all directions. Some of the energy scattered back is absorbed increasing the temperature of the substrate and the coating. For this amount of a scattering the substrate temperature increases with coating thickness as contrast to the substrate temperature decreasing with thickness for a non-scattering coating. For a 0.0127 cm thick layer the temperature drop through the layer is 2.2 K for $k = 3.0 \text{ W/(mK)}$ and 25.2 K for $k = 0.25 \text{ W/(mK)}$. This temperature drop is almost the same as the non-scattering layer. For a 0.127 cm thick layer, the temperature drop through the layer is 11.6 K for $k = 3.0 \text{ W/(mK)}$. This is about 55% of the temperature drop for the non-scattering layer. For $k = 0.25 \text{ W/(mK)}$, the temperature drop is 106.2 K which is 63% of the temperature drop in the non-scattering layer. Scattering causes the temperature drop in a layer to decrease and heat to be retained in the coating and substrate.

The apparent surface temperatures for the low, 0.25 W/(mK), and high, 3 W/(mK), thermal conductivity semitransparent coatings are shown in figures 2 and 3. Here the apparent surface temperature is defined as the temperature a pyrometer operating over all wavelengths would measure for the energy emitted by a gray layer. For the layer with no scattering, figure 2, the apparent temperature (dashed and dots-dashed lines) is closer to the substrate temperature than the surface temperature. For a coating with scattering, figure 3, the apparent temperature (dashed line) is considerably lower than the substrate temperature. Scattering lowers the apparent surface temperature. To obtain the most accurate temperature measurement with an optical pyrometer, a wavelength where the coating is opaque has to be used.

EFFECTIVE THERMAL CONDUCTIVITY

An effective thermal conductivity was determined assuming that all the heat transfer into the layer by convection was conducted to the substrate. So, $q_{\text{convection}}$ equals $q_{\text{conduction}}$. The heat transferred by convection is

$$q_{\text{convection}} = h \times (T_{\text{gas}} - T_{\text{surface}})$$

The effective thermal conductivity is

$$k_{\text{effective}} = \frac{q_{\text{conduction}} \times D}{T_{\text{surface}} - T_{\text{substrate}}}$$

The surface and substrate temperatures calculated previously using the two-flux solution were used to determine the effective thermal conductivity. The effective thermal conductivities and the percent difference between the effective thermal conductivity and the intrinsic thermal conductivity used in the two-flux calculation are in figures 4 and 5. The dotted line in the figures is for $k_{\text{effective}} = k_{\text{intrinsic}}$ and is presented as a reference. The effective thermal conductivities are larger than the intrinsic thermal conductivities. The 0.0127 and 0.0254 cm thick layer data are not presented in the figures. For these thicknesses the percent difference between the intrinsic and effective thermal conductivities was less than 5% for the conditions used. The effective thermal conductivities increase with the thickness of the layer. The largest percent differences between the effective and intrinsic thermal conductivities occur for the thickest layers and the lowest intrinsic

thermal conductivities. The heat conducted through the layer to the substrate is opposite to the net radiative heat flow to the surroundings. The radiative energy scattered back to the substrate will cause the scattering layer to have a higher substrate temperature than the non-scattering layer. This results in a higher effective thermal conductivity in the scattering layer as shown in figure 5.

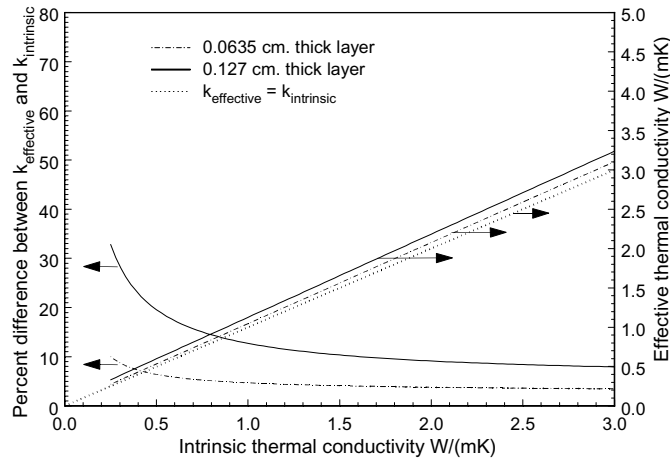


Fig. 4 Intrinsic and effective thermal conductivities non-scattering layer $a = 0.3 \text{ cm}^{-1}$, $\sigma_s = 0$, $\epsilon_b = 0.8$, $n = 2.1$, $T_g = 1600\text{K}$, $T_s = 295\text{K}$

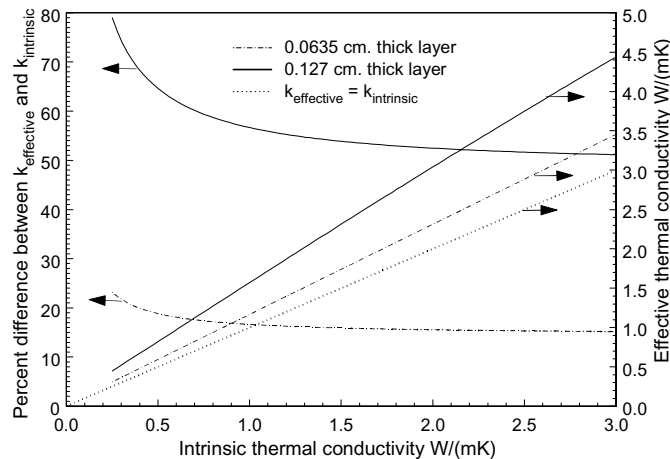


Fig. 5 Intrinsic and effective thermal conductivities scattering layer $a = 0.3 \text{ cm}^{-1}$, $\sigma_s = 100 \text{ cm}^{-1}$, $\epsilon_b = 0.8$, $n = 2.1$, $T_g = 1600\text{K}$, $T_s = 295\text{K}$

In Tables I and II the effect of changing the gas or surroundings temperatures, or the substrate emissivity is investigated for two layer thicknesses. For the 0.0127 cm (0.005 in.) non-scattering and scattering layers, changing the gas or surroundings temperature by 500 K or the emissivity to 0.2 had a slight effect on the effective thermal conductivity. For the 0.127 cm thick layer these changes have a significant effect on the effective thermal conductivity especially for the scattering layer. The lowest percent difference between the intrinsic and effective thermal conductivities was 20.1% for decreasing the gas temperature by 500 K for the non-scattering 0.127 cm thick layer. The greatest percent difference was 91.4% when the substrate emissivity was decrease to 0.2 for the scattering layer.

Table I Effect of gas temperature, surrounding temperature or substrate emissivity non-scattering layer
 $a=0.3 \text{ cm}^{-1}$ $n=2.1$

Thick- ness cm	T _{gas} K	T _{surround} K	ϵ_b	T _{surface} K	T _{substrate} K	k _{intrinsic} W/(mK)	k _{effective} W/(mK)	Percent Difference in k
0.0127	1600	295	0.8	1070.66	1044.00	0.25	0.2522	0.88
0.0127	1100	295	0.8	864.19	852.30	0.25	0.2519	0.76
0.0127	1600	795	0.8	1123.55	1099.57	0.25	0.2523	0.92
0.0127	1600	295	0.2	1151.36	1129.38	0.25	0.2592	3.68
0.127	1600	295	0.8	1156.95	987.49	0.25	0.3320	32.80
0.127	1100	295	0.8	898.51	813.28	0.25	0.3002	20.08
0.127	1600	795	0.8	1202.51	1055.55	0.25	0.3435	37.40
0.127	1600	295	0.2	1177.56	1036.21	0.25	0.3798	51.92

Table II. Effect of gas temperature, surrounding temperature or substrate emissivity scattering layer
 $a=0.3 \text{ cm}^{-1}$ $n=2.1$ $\sigma_s=100 \text{ cm}^{-1}$

Thick- ness cm	T _{gas} K	T _{surround} K	ϵ_b	T _{surface} K	T _{substrate} K	k _{intrinsic} W/(mK)	k _{effective} W/(mK)	Percent Difference in k
0.0127	1600	295	0.8	1096.68	1071.44	0.25	0.2533	1.36
0.0127	1100	295	0.8	880.85	869.85	0.25	0.2530	1.24
0.0127	1600	795	0.8	1144.75	1121.95	0.25	0.2536	1.44
0.0127	1600	295	0.2	1166.96	1145.84	0.25	0.2604	4.16
0.127	1600	295	0.8	1225.66	1119.43	0.25	0.4475	79.00
0.127	1100	295	0.8	949.20	902.51	0.25	0.4102	64.08
0.127	1600	795	0.8	1257.00	1161.24	0.25	0.4549	81.96
0.127	1600	295	0.2	1230.12	1131.94	0.25	0.4785	91.40

CONCLUSIONS

Thermal radiation can play a significant role in the heat transfer in semitransparent coatings. A parametric study was performed to obtain an understanding of radiation effects in a burner rig test of a TBC. A one dimensional model is used. The coating is heated by a hot gas flowing over its surface and cooled by radiating to the surroundings. There is no heat transfer through the backside of the material which simulates a symmetric centerline boundary condition for the specimen. An absorption coefficient of 0.3 cm^{-1} and scattering coefficients of 0 (no scattering) and 100 cm^{-1} (isotropic scattering) were used. The coating is assumed to be gray, that is the properties are not a function of wavelength. The thickness and thermal conductivity of the layer are varied. The results show that the heat transfer is a function of the optical properties of the coating and the substrate. Increasing the thermal conductivity or decreasing the layer thickness results in a smaller temperature drop in the layer. Scattering increases the temperature level in the coating and substrate and decreases the temperature drop through the coating. With no scattering, the substrate temperature decreased with thickness. With scattering, $\sigma_s = 100 \text{ cm}^{-1}$, heat is trapped in the coating, causing the substrate temperature to increase with thickness. An effective thermal conductivity can be significantly different from the intrinsic thermal conductivity for thick scattering TBCs. If an optical pyrometer is used for temperature measurements, the material must be opaque at the measurement wavelength if accurate results are to be obtained.

Appendix A

The equations in ref. 7 were used. The differential equation for the temperature distribution in the absorbing, emitting, and scattering TBC model used is

$$\frac{dT}{dx} = \pm \left[\frac{2\kappa}{k} (1.0 - \Omega) \left\{ \frac{4}{5} n^2 \sigma [T^5(x) - T^5(0)] + \frac{3}{2} \kappa [T^2(x) - T^2(0)] - 3C\kappa [T(x) - T(0)] \right\} + \left\{ \frac{h}{k} [T_g - T(0)] \right\}^2 \right]^{\frac{1}{2}} \quad (1)$$

where σ is the Stefan-Boltzmann constant, $\kappa = (\sigma_s + a)$, $\Omega = \sigma_s/\kappa$, and

$$C = kT(0) + \frac{1}{3K} \left\{ 4 \frac{1 - \rho^o}{1 - \rho^i} q_r^o + 2 \frac{1 + \rho^i}{1 - \rho^i} h [T_g - T(0)] \right\} \quad (2)$$

For surface heating a positive value of the square root is used.

For optically thin layers, there is a temperature gradient at the interface between the TBC and substrate, and the boundary condition at $x = D$ is

$$\left. \frac{dT}{dx} \right|_{x=D} = \frac{1}{k} \frac{2\varepsilon_b}{2 - \varepsilon_b} \left[\frac{3}{4} C\kappa - \frac{3}{4} \kappa kT(D) - n^2 \sigma T^4(D) \right] \quad (3)$$

If the layer is optically thick the temperature gradient is only near the gas-TBC interface and the boundary condition at $x = D$ becomes

$$\left. \frac{dT}{dx} \right|_{x=D} = 0 \quad (4)$$

To obtain the temperature distribution in the layer, the temperature of the surface of the TBC, $T(0)$, is assumed. Equation (1) for dT/dx is solved using a Runge-Kutta method. The boundary condition dT/dx at $x = D$, equation (3) or (4) is checked to see if it is satisfied. If it is not satisfied $T(0)$ is adjusted until the boundary condition is satisfied.

The equation for the apparent surface temperature of the layer, which is the temperature a pyrometer would measure for the emitted energy, can be written as

$$T_{app} = \frac{1}{\sigma^{\frac{1}{4}} (1 - \rho^o)^{\frac{1}{4}}} \left\{ q_r^o (1 - \rho^o) + h [T_g - T(0)] \right\}^{\frac{1}{4}} \quad (5)$$

The interface reflection and transmission were determined using integrated averages of the Fresnel relations ref. 8 page 115.

$$\begin{aligned}\tau^o(n) = 1 - \rho^o(n) = & \frac{1}{2} - \frac{(3n+1)(n-1)}{6(n+2)^2} - \frac{n^2(n^2-1)^2}{(n^2+1)^3} \ln\left(\frac{n-1}{n+1}\right) \\ & + \frac{2n^3(n^2+2n-1)}{(n^2+1)(n^4-1)} - \frac{8n^4(n^4+1)}{(n^2+1)(n^4-1)^2} \ln(n)\end{aligned}\quad (6)$$

This assumes the medium is a non-attenuating dielectric, that is the complex part of refractive index is neglected. This is a reasonable assumption if the absorption is not large ref. 9. The complex part of the refractive index determines the absorption coefficient. If the absorption coefficient is large the complex index of refraction must be included in the relations for the reflectivity and transmission of the interface.

The internal reflection, which includes energy at angles greater than the critical angle for total reflection is ref. 10

$$\rho^i(n) = 1 - \frac{\tau^o(n)}{n^2} \quad (7)$$

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